

# Experiences on nitrogen removal from liquid fraction of pig slurry using the SBR technology

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An overview on the use of the SBR technology for N-removal from liquid fraction of pig slurry by means of nitrification-denitrification is presented. Laboratory-, pilot- and full-scale experiences have been collected and typified. The composition of piggery wastewaters may vary widely depending on factors such as geographical area, management, pre-treatments, etc., circumstances that affect the operation and performance of a SBR system. The compiled experiences showed that SBR is a flexible and mature technology to properly deal with nitrogen removal under very different situations.

**Keywords:** Nitrification-denitrification (NDN); Sequencing batch reactor (SBR); Piggery wastewaters; Nitrogen surplus

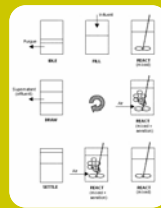
## Nitrogen surplus derived from intensive pig farming

Slatted floors in farming has led to the production of livestock slurries with low dry matter content. The use of these slurries as organic fertilizer is the most adequate option but when slurry generation is larger than crop needs a problem of nutrient surplus appears. Under these circumstances, complementary treatment strategies have to be considered. Up to 50-60% of the total nitrogen initially present in a pig slurry is susceptible of being biologically eliminated through NDN.



## Sequencing Batch Reactor technology

A conventional SBR consist on an activated sludge system operated with a fill and draw sequence [cycle], which is repeated over time



## Raw Liquid Fraction of Pig Slurry (LFPS)

- High compositional variability within regions, farms or seasons and also due to the separation device used
- TS content 0.5-2.5%
- Variable BOD/COD ratio. BOD mainly attributed to slowly biodegradable organic compounds
- High N concentration is expected in both, ammonium and organic forms, although  $\text{NH}_4\text{-N}$  is dominant (~70%).
- Presence of other nutrients (P and K), certain heavy metals (Cu and Zn) and other ionic species which confers a significant electric conductivity
- Presence of pathogens

## LAB-SCALE



Reference	LFPS	External Org. C supply	Operation				Influent ( $\text{g l}^{-1}$ )			Removal (%)					
			NLR ( $\text{g l}^{-1} \text{d}^{-1}$ )	HRT (d)	SRT (d)	CL (h)	Dry. C	N	P	Dry. C	N	P			
Wun-Jern (1989)	R+D/AD	No	0.27-0.44	1.3	∞	24	3.16	0.5	3.5	2.19-2.79	0.35-0.55	48-58	86-2	-	
Fernandes and McKees (1991)	R	No	0.15-0.40	3-9	10-30	24	3.19	0.5	0.5	25.93-2.0	1.00-1.40	81-97	<35-54	-	
Fernandes et al. (1991)	R	No	0.14-0.20	6-9	20	24	3.9-10.0-9.1	1.0-5.0-5.0	0.5	30.7-31.2	2.41-2.58	95-97	80-93	-	
Dasari et al. (1991)	R+D	No	0.05-0.22	3	17-19	24	0.51	1.1	2.0-5.0	1.50-2.25	0.29-0.67	0.08-0.24	81-96	72-98	19-91
Bortone et al. (1992)	R	No	0.13	10	28-34	24	6.7	4.0	0.8-0.2	10.6	1.26	0.24	93	88-93	95
Matsuda et al. (1995)	R+P	No	0.08	1.2	-	24	3.2	0.0	0.1	8.0	1.17	0.11	-	91	-
Andreatola et al. (1997)	R	No	0.21	10	30	24	[3.3 4.2]	1.5	0.0	19.1	2.06	-	98	-	-
Lee et al. (1997)	R+D	Yes	0.07	2	19	24	0.2	0.2	0.2	2.95	0.15	0.05	96	NH <sub>4</sub> -N	89
Magrí and Flotats (2000)	R	No	0.13	21	20	24	6.8	5.4	0.8-0.2	18.7	2.67	1.05	98	99	-
Kishida et al. (2003)	R+C	No/Yes	0.11-0.13	10	45-500	8	3.2	4.0	0.1	2.99-5.32	1.19-1.25	0.09-0.10	92-100	51-95	-
Obaja et al. (2003)	AD+D	Yes	0.91-1.65	1	11	8	2.4	1.1	0.0	2.26-3.97	0.91-1.65	0.09-0.15	64-70	-100-97	95-98
Chen et al. (2004)	R+C	No/Yes	-0.11-0.07	-6.3-10	-	Variable	0.1	Var	0.0-0.1	2.91	0.71	0.03	99-100	81-95	18-55
Kim et al. (2004)	pAD	No	0.11-0.22	20-40	-	-	7.16-5.4	5.12-1.3-2	0.0	19.5-48.8	4.34-4.82	-	92-97	95-97	-
Kim et al. (2004b)	R+C	Control strategy	-0.10-0.08	-7.5-9	32	-3.4-0.0	0.1	Var	0.0-0.1	3.21	0.72	0.05	56	50	50
Obaja et al. (2005)	AD+D	Yes	1.03	0.9	11	7	1.2	1.1	0.5-0.1 <sup>D</sup>	1.74	0.90	0.08	-	-100	98
Dang et al. (2006)	pAD	No	0.05	3	30	12	2.3	1.1	0.0	2.91	0.79	-	90	-	-
Zhu et al. (2006)	R+D	No/Yes	0.37	3.3	21	8	1.25	2.75	1.2-5.0	8.80	1.22	0.60	98-97	96-99	68-87

## LARGE-SCALE



Reference	LFPS	External Org. C supply	Operation				Influent ( $\text{g l}^{-1}$ )			Removal (%)					
			NLR ( $\text{g l}^{-1} \text{d}^{-1}$ )	HRT (d)	SRT (d)	CL (h)	Dry. C	N	P	Dry. C	N	P			
Wong and Choi (1998)	R	No	0.08	9	9-12	24	2.18	4.2	0.1	2.88	0.70	-	>98	-	-
Lo et al. (1991)	R+D	No	0.34	1	14	4	0.1	3.3	0.5-0.1	2.35	0.33	-	52	0	-
Saeed et al. (1997)	R	No	0.09	3	-	24	0.5	[3.2]	0.5	3.77	0.28	0.26	89	35-53	51
Bicudo et al. (1999)	R	No	0.13-0.24	5-10	30-35	12-24	[1.1], [1.4-1.1], [2.2]	0.0	0.0	3.60-8.20	1.10-1.30	0.15-0.20	65-93	75-95	15-70
Saeed et al. (1999)	pAD	No	-	3	-	24	0.75	[1.5]	1.25	0.42	-	-	44	47-65	-
Tilche et al. (1999)	R	No	0.12	5.7	15	24	[2.2]	1.5-2.5	0.0	6.46	0.70	0.09	98	98	98
Edgerton et al. (2000)	R	No	0.08	6.7	30	9.5	0.25	3.5	1.0-2.5	4.50	0.55	0.06	79	-100	49
Choi and Eum (2002)	R	No	0.10-0.20	54	54	24	8.16	45.3	6.68	0.67	-	-	[30-50]	-	-
Poo et al. (2004)	R/AD	Yes	0.35-0.22	10-25	-	24	[1.5]	1.3-1.4	0.0	47.5-11.0	4.75-3.70	0.10-0.03	98-98	-	-
Poo et al. (2005)	R	Yes	0.14-0.43	27-9	Variable	Variable	[1.7]	1.1	0.0	11.0	3.80	0.02	-	-100	-

**Nomenclature.** NLR: nitrogen loading rate; HRT: hydraulic residence time; SRT: solids residence time; CL: cycle length; F: fill; AF: anoxic fill; OF:oxic fill; AFR: anoxic/anaerobic fill; AFR: anoxic/anaerobic fill and react; AFR: anoxic/anaerobic instantaneously fill and react; OFR:oxic fill and react; AR: anoxic/anaerobic react; AR: anoxic/anaerobic react with external carbon addition; OR:oxic react; S: settle; D: draw; ID: instantaneously draw; AI: anoxic/anaerobic idle; n: times that a sequence is repeated; Var: Variable; LFPS characteristics: R: raw; D: diluted; AD: anaerobically digested; pAD: partially anaerobically digested; P: precipitated; C: coagulated. **N removal.** Also including N oxidized forms, over liquid effluent.

## "Hot" issues

### Nitrification

- High electric energy consumption linked to aeration
  - 4.57 kg O<sub>2</sub> kg<sup>-1</sup> NH<sub>4</sub>-N on stoichiometric basis
  - 11.3 kWh m<sup>-3</sup> slurry, overall treatment plant (Tilche et al., 1999)

### Denitrification

- Organic carbon requirements (~6 kg BOD kg<sup>-1</sup> N<sub>nitri</sub>)
- High BOD favors aerobic heterotrophic growth, increasing O<sub>2</sub> consumption and may even destabilize the process due to the temperate rise (> 35°C). Advisable to consider a preliminary anaerobic digestion
- Low BOD limits denitrification. Proposed alternatives:
  - addition of an external carbon source
  - (in this context NDN via nitrite may result interesting)
  - partial separation of NH<sub>4</sub>-N by struvite precipitation

### Control performance

- Timers vs. real-time probe measurements
- Minimization of greenhouse gasses emission (NO<sub>2</sub>, CH<sub>4</sub>)

### Engineering

- Based on previous laboratory assays/simulation
- Possibility of upgrading outdated installations

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New biotechnological developments on N-removal that are more energy efficient, such as the PANI-Anammox, might replace treatment strategies based on NDN provided that robustness, flexibility and simplicity are ensured.